

Optimizing the Biofuel Production by Hydrotreating Jojoba Oil

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Abstract

Hydroprocessing of vegetable oils is a prominent technology that using the existing infrastructure of petroleum refineries, for producing environmental friendly and high quality transportation fuel.

In this study, Jojoba oil was hydrotreated , using the conventional Ni Mo/ Al₂O₃ catalyst in the sulfided form .A series of experiments were performed at various conditions in a cata –test unit , to predict the influence of reaction temperature , pressure and liquid hourly space velocity on the yield and quality of the obtained product . The results indicated that hydrotreating process is much more selective for producing hydrocarbons in the gas oil range.

450⁰C, 2.5 MPa and 5 h⁻¹ LHSV were found to be the optimum conditions that generate 84.1 wt % biofuel with a selectivity of 88.37%. These results were confirmed via various analyses such GC, FTIR, ASTM...etc. The hydrotreated product obtained at the best operating conditions was evaluated and reflects the significant improvement of the physicochemical properties of the biofuel attained compared with those of the crude jojoba oil.

Keywords: Green Fuel, Hydrotreated , Jojoba Oil

1. Introduction

In the context of gradual depletion of fossil fuels reserves , and increasing energy demand with ever increasing number of vehicles employing compression ignition engines , makes the implementation of sustainable fuels a crucial issue worldwide (1-2) . Many alternatives that can be derived from sources other than petroleum crude oil have been considered (3). Among these, biofuels, that received a great attention as an alternative, since it contains no sulfur, nontoxic, biodegradable and renewable fuel.

Recently, there are several studies on the production of biofuel from utilization of biomass substrates, waste oil, vegetable oils and animal fats, ...etc, that can serve as a partial substitute for fossil fuels (4-8).

Plant oils, such as sunflower, corn, rapeseed, palm oils ...etc, can be visualized as a promising sources for biofuel production (9-11). Consequently, the demand of this type of oils is expected to noticeably increase in the next few years. However, the intensive use of biofuels come from vegetable oils could derive in a shortage of raw materials for feed purposes and a steep rise of food price. This situation could be avoided by the use of less – valuable feedstocks such as waste cooking oils or non – edible oils (12-14). In this investigation the non- edible oil extracted from jojoba seeds has been chosen and evaluated as an appropriate feedstock for biofuel obtainment.

The most commonly used method for biofuel, particularly biodiesel production, is the transesterification of triglycerides with an

alcohol (methanol / ethanol) using basic or acid catalysts, producing glycerol as a secondary product (15-18). Nevertheless, vegetable oils can also be converted to liquid hydrocarbon fuels using catalytic technology (19-21) such as cracking and hydroprocessing techniques that regarded as the most reasonable and promising technologies for high yield of liquid products .

The objective of the present research is to optimize the process operating conditions for the production of petroleum–like fraction (particularly biodiesel) from jojoba oil via hydrotreating technology using Ni Mo/ Al₂O₃ catalyst.

2. Experimental

2.1 Feedstock

Jojoba oil purchased from Egyptian Company for Natural Oil has been used as a feedstock.

2.2 Catalyst preparation

In this study, the conventional hydrotreating Ni Mo/ Al₂O₃ catalyst (HR-348) procatalyse Co, was employed. The catalyst was calcined at 400 ⁰C for 6 hrs, and then presulfided with 2 wt % dimethyl disulfide (DMDS) in n- hexane mixture. Sulfidation was performed at 2 different temperatures. The first sulfidation has done at 260 ⁰C for 3 hrs and the second was carried out at 360 ⁰C also for 3 hrs.

2.3 Catalytic activity measurements

Hydrotreatment of jojoba oil was processed using a continuous high pressure micro-reactor (cata-test unit). A detailed description of the

apparatus was given elsewhere (22). The sulfided Ni Mo/ Al₂O₃ catalyst mixed with the same volume of ceramic, was loaded in the middle zone of a stainless steel tubular reactor (1.9 cm i.d. and 50 cm in length), equipped with electric heating. H₂ gas was supplied to the unit from a H₂ cylinder, while liquid feed was pumped at the top of the reactor by means of a piston pump having an adjusting knob. The experiments were accomplished at reaction temperatures in the range of 375- 500 °C, and LHSV of 1-5 h⁻¹ under H₂ pressures of 1-5 MPa.

The effluent gases and liquids were collected and estimated. The organic fraction, separated from water that involved in the liquid product, were analyzed according to the different ASTM method: Density (D- 287), kinematic viscosity (D- 455), sulfur content (D-4294), using X- ray fluorescence sulfur meter, ASTM distillation (D -86). More evaluation for the virgin oil and the hydrotreated organic product, obtained at 450 °C, LHSV of 5h⁻¹ and 2.5 MPa H₂ pressure, were carried out, including the determination of pour point (D-97), molecular weight (D-2502), calorific value (D-240), refractive index (D-1747), ash content (D- 482) and flash point (D-92), beside the analyses via GC and FTIR technique. The gas chromatographic apparatus, Agilent 6890, equipped with flame ionization detector (FID) has been employed. Separations were performed on HP-1 column with 30 meter length and 0.25 mm ID. The temperature of the injector and detector were set at 300 °C. FTIR spectroscopy was determined using Nicoletis-LOFT-IR Nicolet 15-10.

3. Results and discussion

3.1 Effect of reaction temperature:

To optimize the operating conditions for the hydrotreating process to produce liquid biofuel from jojoba oil several approaches have to be examined. Reactor temperature is visualized as one of the most significant parameter affecting the catalyst performance. Therefore, the influence of this factor on the quality and quantity of the hydrotreated jojoba oil has been explored.

The present study took place at four different reaction temperatures, in the range of 375- 500 °C, at constant experimental conditions i.e. (5h⁻¹ LHSV, 2.5 MPa hydrogen pressure and 1600 L/L H₂ / feed ratio), using sulfided Ni Mo/ Al₂O₃ catalyst. The obtained results are declared in Table 1. The reported data reflect a sharp increase in the converted yield from 48.81 to 85.59 wt%, particularly upon raising the reactor temperature from 375°C up to 400°C, beyond which the total

conversion is considerably improved to attain a value of 95.23 wt% at 450°C. At more elevated temperatures, i.e. 500°C, the influence of this factor on the amount of the transformed feed become insignificant. It worth mentioning that we found difficulties for carrying out the experiments at temperatures below 375°C due to the transformation of the products to waxy constituents that cannot be easily collected and makes some troubles to the apparatus used. This phenomenon may be ascribed to the hydrogenation of the double bonds involved in the structure of jojoba molecules, forming saturated oil that cannot be easily fragmented, since such low temperature applied is not enough to promote the disconnection between their bonds.

Table 1 shows also that, moderate amounts of the effluent gases resulted from the hydrotreating process, comprised 6.47 – 11.64 wt%, were observed throughout the whole range of temperature applied. Although the high temperatures suit the procession of hydrocracking reaction due to its endothermicity, however, the formation of gases and light fractions are not so intensive here since the used Ni Mo/ Al₂O₃ catalyst has not enough strong acid sites to promote a server cracking of molecules, compared to other acidic catalyst such as zeolite as an example.

Nevertheless, somewhat enhancement of gas formation with temperature accompanied by slight diminutions of the liquid yield (which composed mainly from organic and some aqueous components) could be observed. After separating the oil from the contaminated water, involved in the liquid yield, it could be noticed that, the products achieved at higher reaction temperatures include relatively more water, on the account of the oil content, than those obtained at lower temperatures. This may be attributed to enhancement of the rate of dehydration reaction which is more favored at elevated temperatures.

Distinct drops in both density and kinematic viscosity of the produced oil are realized with exceeding the reaction temperature, due to the procession of hydrotreating that accompanied by hydrocracking reaction.

To determine the boiling range distribution of the organic liquid products which accomplished at various reaction temperatures, ASTM distillation has been implemented and the accessible data were also depicted in Table1. The conversion to biofuel is considered to be the amount of distillates possessing a lower boiling point than that of the crude jojoba oil which has been determined here and found to be > 323°C.

It is obvious from the ASTM results that unsatisfactory transformation to petroleum-like fractions, not exceed than 45 vol % of the produced oil has been achieved at 350°C. The remainder represents unconverted oil, residue and losses. At higher temperatures, substantial quantities of the required products ranging from 85 to 97 vol % were accomplished. Therefore, the recommended reaction temperature to be applied in hydrotreating jojoba oil is 450 °C, in order to acquire the highest activity with good selectivity to biofuel production.

Moreover, the biofuel obtained at various reaction temperatures were fractionated and

separated to three portions according to their boiling ranges, i.e. (IBP-150 °C), (150 – 250 °C) and (250 – 323°C), for gasoline kerosene and gas oil, respectively. Generally, it could be noticed that reaction temperature has some influence on the percentages of each of the forementioned fractions which involved in the distillates under investigation. As evidenced from Figure1 that diesel – like fraction is the most prevalence distillate particularly at 400 and 450 °C that comprised 55 vol% of the biofuel acquired.

Table 1. Distribution of the Hydrotreated Products Obtained at Various Temperatures Pressure: 2.5 MPa, L.H.S.V.: 5 h⁻¹ and H₂ / feed: 1600 L/L

Hydrotreated Products	375 °C	400 °C	450 °C	500 °C
Total conversion , wt %	48.805	85.587	95.23	96.88
Hydrotreated product , Wt %				
Gases	6.47	7.46	7.51	11.64
Liquid	93.53	92.54	92.49	88.36
Water content	1.04	1.45	3.62	3.98
Oil content	92.49	91.09	88.87	84.38
Density at 20 °C	0.8595	0.820	0.8065	0.7017
Kinematic viscosity at 40 °C	22.0679144	16.093376	3.695354	1.925515
Sulfur content , ppm	0.007	0.006	0.006	0.003
ASTM distillation, vol. %/ °C				
IBP	110	60	60	60
10	110	100	100	100
20	258	160	155	120
30	303	199.8	179.8	150
40	313.7	250.6	231.8	199.8
50	324.4	284.4	256.6	231.6
60	324.4	284.4	252.7	231.6
70	324.4	284.4	284.4	284.4
80	324.4	305.3	305.4	284.4
90	324.4	325.9	305.4	294.9
FBP	324.4	325.9	305.4	294.9
Biofuel recovered, vol. %	45	85	95	97
Unconverted , residue , and Loss , vol. %	55	15	5	3
Biofuel yield , wt % based on feed	41.295	76.68	84.1	81.26
Biofuel selectivity , %	84.61	89.589	88.37	83.87

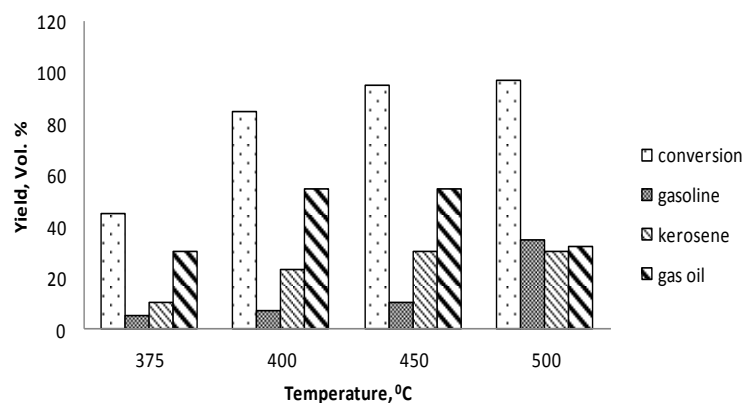


Fig 1. Distribution of the individual fractions of the biofuel obtained as a function of Temperature.

3.2 Effect of liquid hourly space velocity (lhsv)

Jojoba oil was hydrotreated at 450°C, 2.5 MPa hydrogen pressure and various liquid hourly space velocities (LHSV), in order to examine the effect of this parameter on the yield and quality of the produced constituents.

The data represented in Table 2 reveals a slight enhancement of the total conversion as the LHSV increased from 1h⁻¹ to 2.5h⁻¹, beyond which a significant improvement has been achieved. A considerable influence of space velocities on the distribution of the products can be observed.

At lower LHSV (i.e. 1h⁻¹), substantial amount of gases comprised around 30 wt% was released, which can not be considered, in this work, as a biofuel product. Simultaneously, low yield (amount to 66.16wt %) of oil was produced compared to 83.25 and 88.87wt% that accomplished at higher space velocities. Undoubtedly, this ascribed to the development of cracking process that favored with increasing the contact time.

It could be recognized that, the product obtained at LHSV of 1h⁻¹ constitutes mainly from appreciable amount of gases contaminated with high boiling point liquid. This could be explained in terms that sever cracking took place at such suitable conditions of high temperature and long contact time, leading to formation of gases and light olefinic compounds followed by fast polymerization of most of these unsaturated fragments giving rise to fraction with high boiling points.

Generally, the reaction products exhibit perfect values of density and kinematic viscosity, particularly for these performed at relatively higher LHSV; also the data indicate the absence of sulfur.

According to the ASTM results (Table2), a distinct amelioration in both the yield and biofuel selectivity has been accomplished as the LHSV increased above 1h⁻¹, remembering that the liquid fraction with boiling point higher

than 323°C is considered to be as unconverted oil. Although the biofuel selectivity achieved at LHSV of 2.5 and 5h⁻¹ are nearly similar, however, a higher yield of biofuel was attained at 5h⁻¹ that characterized by the predomination of fraction in the diesel range, whereas that achieved at 2.5h⁻¹ is distinguished by the prevalence of the middle distillate in the kerosene and diesel range associated with some polymerized components Figure 2. Therefore, 5h⁻¹ LHSV is recommended to carry out the further experiments.

3.3 The effect of hydrogen pressure

The effect of hydrogen pressure factor on the product distribution of the hydrotreated jojoba oil has been explored. Table 3 represents the results of the experiments performed at 450°C, 5h⁻¹ LHSV and 1600 L/L H₂: feed, at various hydrogen pressures.

At a pressure of 1.0 MPa, 70.75 wt% of jojoba oil was transformed to 5.14 wt% gas and 94.86 wt% liquid products involving 3.1 wt% water. The gradual increase in pressure to 2.5 MPa and after to 5MPa, was accompanied by conspicuous improvement in the total conversion to come to the values of 95.23 and 98.15 wt% respectively. The data reflect also a moderate stimulation to gas formation with simultaneous drop in the oil content, as the pressure increased from 1 to 5 MPa.

Significant upgrading in both density and kinematic viscosity of the obtained oil has been occurred throughout the whole range of the pressure applied, particularly at 5MPa.

The ASTM data reported in Figure 3 reveals the unsatisfactory results shown at low hydrogen pressure. Nevertheless, upon raising the pressure up to 2.5 and 5MPa, a sharp increase in the quantities of the aquired biofuels has been realized, at which the activity to biofuel production are nearly the same. Therefore, 2.5 MPa hydrogen pressure can be recommended for processing the oil, since it

consumes less hydrogen, moreover, it gives better selectivity than that performed at 5MPa.

Regarding to the distribution of the three fractions mentioned previously, the best yield of diesel fraction can be acquired at a pressure of 2.5 MPa that amounts to 55 vol% of the oil product, where as the rest represent 30 vol% kerosene, 10 vol% in the range of gasoline and

5 vol% unconverted oil and losses. This distribution varies at 5 Mpa, at where the amount of diesel diminished to 33 vol% with consequent increase in gasoline to become 35 vol% due to cracking reaction and transformation of apart of diesel to the lighter fraction.

Table 2. Distribution of the Hydrotreated Products Obtained at Various LHSV. Temperature: 450 0C, Pressure: 2.5 MPa and H2 / feed: 1600 L/L

Hydrotreated Products	1 h⁻¹	2.5 h⁻¹	5 h⁻¹
Total conversion , wt %	85.98	86.665	95.23
Hydrotreated product , Wt %			
Gases	29.83	12.88	7.51
Liquid	70.17	87.12	92.49
Water content	4.01	3.87	3.62
Oil content	66.16	83.25	88.87
Density at 20 °C	0.8173	0.8100	0.8065
Kinematic viscosity at 40 °C	5.958485	4.3324092	3.695354
Sulphur content , ppm	0.0012	0.0049	0.006
ASTM distillation, vol. %/ °C			
IBP	80	80	60
10	120	120	100
20	205.6	160	155
30	227.0	194.1	179.8
40	280.3	205.6	231.8
50	312.0	227.0	256.6
60	312.0	248.4	252.7
70	312.0	290.9	284.4
80	312.0	305.3	305.4
90	325.9	325.9	305.4
FBP	325.9	325.9	305.4
Biofuel recovered, vol. %	80	85	95
Unconverted , residue and Loss , vol. %	20	15	5
Biofuel yield , wt % based on feed	52.14	69.915	84.1
Biofuel selectivity , %	60.64	86.73	88.37

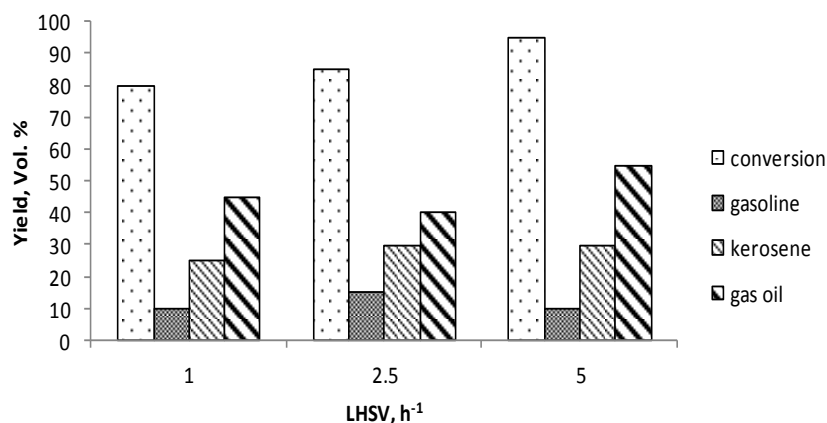


Fig 2. Distribution of the individual fractions of the biofuel obtained as a function of LHSV.

Table 3. Distribution of the hydrotreated Products Obtained at Various H₂ Pressure. Temperature: 450 °C, LHSV : 5h⁻¹ and H₂ / feed: 1600 L/L

Hydrotreated Products	1.0 MPa	2.5 MPa	5.0 Mpa
Total conversion , wt %	70.75	95.23	98.15
Hydrotreated product , Wt %			
Gases	5.14	7.51	10.93
Liquid	94.86	92.49	89.07
Water content	3.10	3.62	3.93
Oil content	91.76	88.87	85.14
Density at 20 °C	0.8140	0.8065	0.7959
Kinematic viscosity at 40 °C	4.132674	3.695354	3.358297
Sulpher content , ppm	0.0052	0.0060	0.0034
ASTM distillation, vol. %/ °C			
IBP	60	60	60
10	160	100	100
20	250.8	155	120
30	284.4	179.8	150
40	305.4	231.8	199.4
50	305.4	256.6	231.6
60	305.4	252.7	250.3
70	305.4	284.4	284.4
80	325.9	305.4	284.4
90	325.9	305.4	305.4
FBP	325.9	305.4	305.4
Biofuel recovered, vol. %	70	95	98
Unconverted , residue and Loss , vol. %	30	5	2
Biofuel yield , wt % based on feed	62.51	84.1	83.29
Biofuel selectivity , %	88.35	88.37	84.86

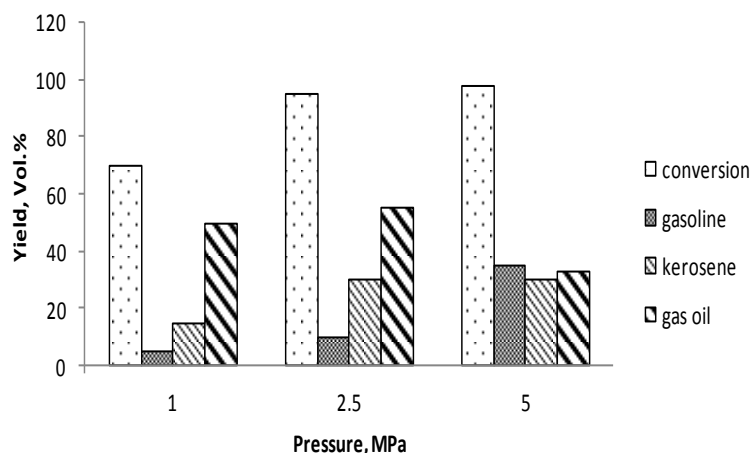


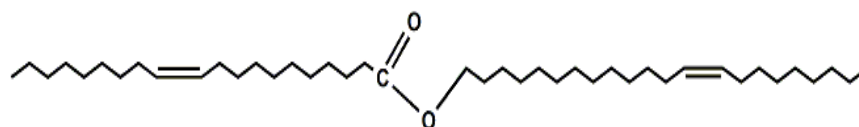
Fig 3. Distribution of the individual fractions of the biofuel obtained as a function of Pressure.

3.4 Gas chromatography

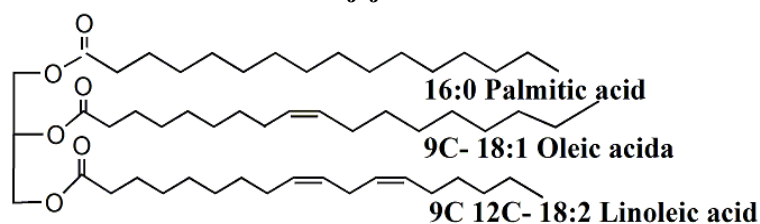
The gas chromatographic chart of jojoba oil shows that , the virgin oil composed mainly from heavy straight chain components including more than 16 carbon atoms per molecule , particularly in the range of C_{40} - C_{42} (Figure 4a). Most of the raw jojoba oil constitute principally from linear wax esters, the remainder comprises free fatty alcohols and acids. About 70% of the esters present are

combinations of acids and alcohols that are predominantly 20- 22 carbon atoms long. (23)

In contrast, common vegetable oils are supplied as triglycerides that can be seen as the condensation of glycerol and three fatty acids whose carbon chain lengths are mostly 16 and 18, with varying degree of unsaturation (24). A comparison between the structure of both jojoba oil and vegetable oils can be illustrated as follows:



Structure of jojoba oil



Example of triglyceride structure

The gas chromatographic spectrum obtained after hydrotreating the crude jojoba oil at 450 °C, 5 h⁻¹ LHSV and 2.5 MPa hydrogen pressure over sulfided Ni Mo/ Al₂O₃ catalyst indicates the disappearance of the peaks corresponding to the high boiling constituents of the feed as declared in Figure 4b. Instead, the produced oil

was enriched with straight chain molecules, most of which posses 20 or 22 carbon atoms that lie in the diesel range. These results are compatible with those attained from the distribution of the distillation range of the product as depicted in Table 3 and Figure 3.

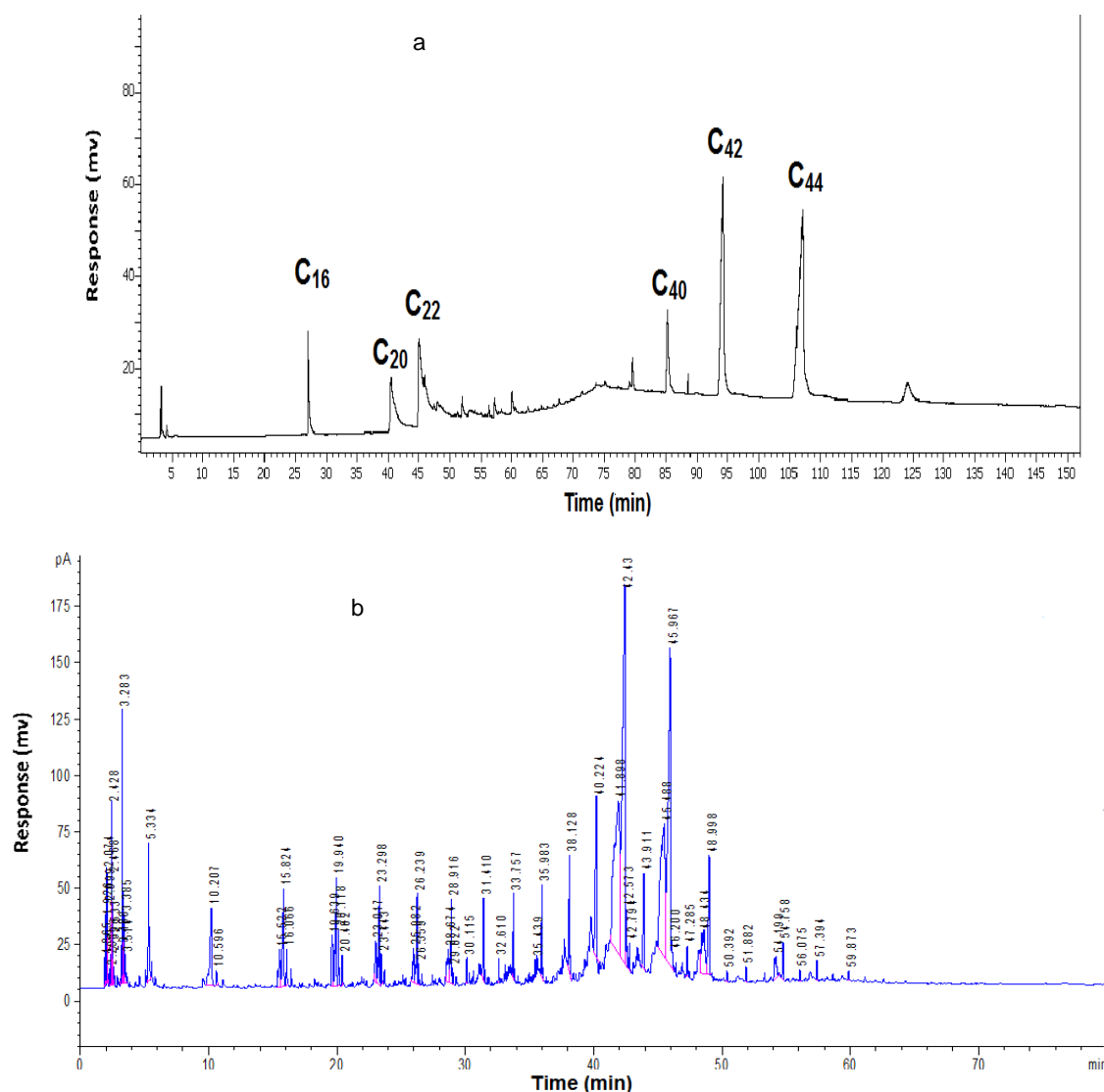


Fig 4. Gas chromatography for (a) Virgin jojoba oil (b) Hydrotreated jojoba oil at 425⁰C.

3.5 Forier transform infra red (ftir) spectroscopy

The Forier transform infrared spectra of Jojoba oil and the hydrotreated product obtained at 450⁰C, 2.5 MPa and 5 h⁻¹LHSV are represented in figure 5 a and b. The recorded spectrum of the feed reveals the predomination of aliphatic components as evidenced from the appearance of strong peaks attributed to alkane C-H stretching vibration at 2857-3000 cm⁻¹. Absorption bands were also observed at 1359 and 1457 cm⁻¹ due to aliphatic C-H bending of methyl and methylene groups. Besides the spectrum exhibits a medium absorption peak at 727 cm⁻¹ related to the out-of-plane bends of alkene.

In addition, the IR spectrum reveals noticeable signals in the oxygenated group regions. The intense C=O stretching band of ester at 1740 cm⁻¹ and those for stretching vibration of C-O at 1150, 1174 and 1255 cm⁻¹

were detected. Moreover weak bands were also observed at 2676 cm⁻¹ and 3410 cm⁻¹ for O-H of carboxylic acid and H – bonded of alcohol, respectively.

Therefore , the IR analysis characterize the crude jojoba oil as being composed of aliphatic ester, most of which are saturated , and associated with some alcohol and carboxylic functional groups.

Analyzing the spectrum of the hydrotreated jojoba oil (Figure 5b), it could be observed the significant diminution in oxygen content compared with that of the feed (Figure 5a). It is obvious that the characteristic stretching band of C=O at 1712 cm⁻¹ has a lower intensity for the obtained product than the corresponding band of crude oil. Also , ratio of the height of this peak and its CH₂ , CH₃ peak heights at 2857-2925 cm⁻¹ in spectrum b, is lower than that of the virgin oil (spectrum 5 a) .

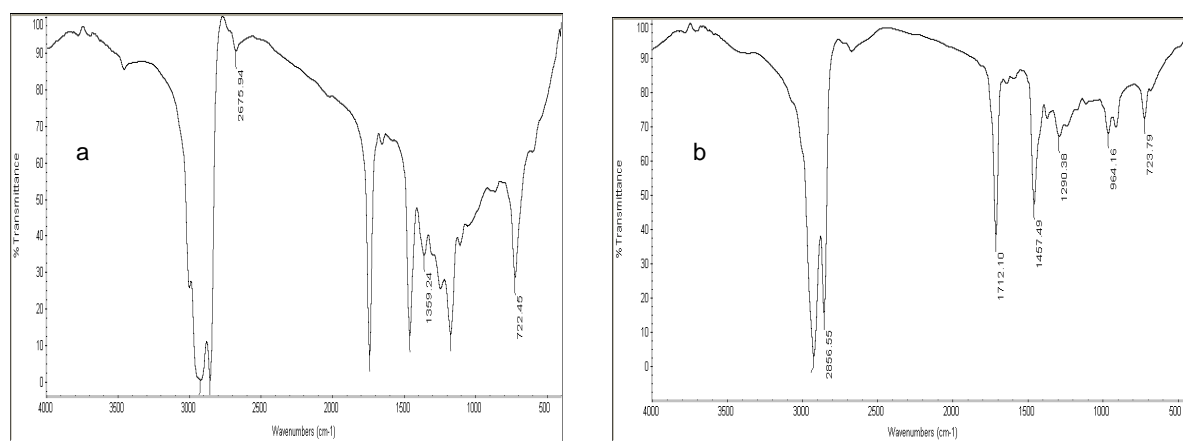


Fig 5. FTIR spectra for (a) Virgin jojoba oil (b) Hydrotreated jojoba oil at 425⁰C.

It could be mentioned that the carbonyl group of ester that appeared at 1740 cm⁻¹ in the original spectrum (5a), was shifted in spectrum (5b) to 1712 cm⁻¹ which is characteristic of a ketonic carbonyl group. Furthermore, the medium intensity absorption at 1150, 1174 and 1255 cm⁻¹ that related to the stretching vibration of C-O shown in spectrum 5a, were significantly reduced in the hydrotreated oil (spectrum 5 b). Also the weak band attributed to O-H group that appeared at 2676 cm⁻¹ (spectrum a) was almost vanished in (spectrum b). Therefore the FTIR analysis gave evidences to the clear reduction occurred in the oxygenated content in the hydrotreated oil.

Besides , the hydrotreatment process was accompanied also by partial saturation of the olefinic bonds as revealed from the weakness of the olefin peak at 723 cm⁻¹ (spectrum b) comparable with the corresponding peak in(spectrum a).

3.6 Evaluation of the crude jojoba oil and the hydrotreated product:

The physicochemical properties of the virgin and hydrotreated jojoba oil were

evaluated, and the results are depicted in table (4) .

The data reflect the pronounced changes of the characteristics of jojoba oil before and after hydrotreatment at 450⁰C, 5 h⁻¹ LHSV and 2.5 MPa hydrogen pressure. It could be observed that, the applied process succeeded in improving most of the important properties of the oil under investigation to be enabled for usage as a biofuel. For instance, a distinct reduction of the density from 0.8650 to 0.8065 as well as an enormous drop in viscosity from 24.9107 to 3.69535 have been occurred. Furthermore, the molecular weight, pour point and refractive index of the attained product were found to be lower than those of the feedstock. Besides, a slight increase in the calorific value of the hydrotreated oil was also achieved, which may be ascribed to the lower value of oxygen of the product with respect to that of the feedstock.

Therefore, these results reveal that, the hydrotreated jojoba oil can be considered as one of the promising and attractive alternative energy from renewable source, in order to meet the great demand of petroleum oil.

Table 4. Physicochemical characteristics of crude and hydrotreated product of jojoba oil

Characteristics	Method	Crud jojoba oil	Hydrotreated jojoba oil product
Density g/ml at 20 ⁰ C	ASTM D- 287	0.8650	0.8065
Kinematic Viscosity , at 40 ⁰ C	ASTM D- 455	24.9107	3.69535
Sulfur content ,ppm	ASTM D- 4294	0.006	0.006
Pour point ⁰ C	ASTM D- 97	9	-15
Molecular weight	ASTM D- 2502	606	211.43
Calorific value, kJol/kgm	ASTM D- 240	45121	45771
Refractive Index at 20 ⁰ C	ASTM D- 1747	1.442	1.42753
Ash content , wt%	ASTM D- 482	Nil	Nil
Flash point , ⁰ C	ASTM D- 92	292	92

4. Conclutions

Hydrotreating process is found to be a promising technique for producing petroleum-like fractions, particularly biodiesel, from the

non-edible jojoba oil, using NiMo/Al₂O₃ catalyst.

The influence of operating variables has been investigated to elucidate the optimum

conditions for attainment the maximum yield of the desired biofuel product.

The total conversion of the feedstock is significantly high at all conditions under investigation, except with that performed at 350°C and 1MPa hydrogen pressure. However the distributions of the obtained yields are qualitatively and quantitatively depend on the applied operating variables.

Sufficient high reaction temperature, pressure and liquid hourly space velocity are favorable for the biofuel production, and vice versa. Furthermore, at such conditions, the hydrotreating process leads to a substantial decrease of both density and kinematic viscosity of jojoba oil to reach the required values.

From the obtained data, it could be concluded that the optimum operating conditions for attainment the highest yield of biofuel, comprised 84.1 wt % with a selectivity of 88.37% are 450°C, 5h⁻¹ LHSV and 2.5 MPa hydrogen pressure.

The acquired biofuel at these circumstances composed from 10 vol% gasoline, 30 vol% kerosene and 55 vol% gas oil, from the obtained liquid oil. The rest represents the loses and unconverted oil

The achieved petroleum-like fractions constitute principally from alkanes, as evidenced from the IR spectrum that indicated the considerable elimination of oxygen from jojoba molecules

After applying the hydrotreating process, a great improvement of the physicochemical characteristics of jojoba oil has been realized in an effort to be used as a renewable fuel alternative to petroleum oil.

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